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## Performance evaluation of *in situ* Fenton-mediated photocatalysis of industrial dye effluent with enhanced TiO<sub>2</sub> nanoparticle

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### ABSTRACT

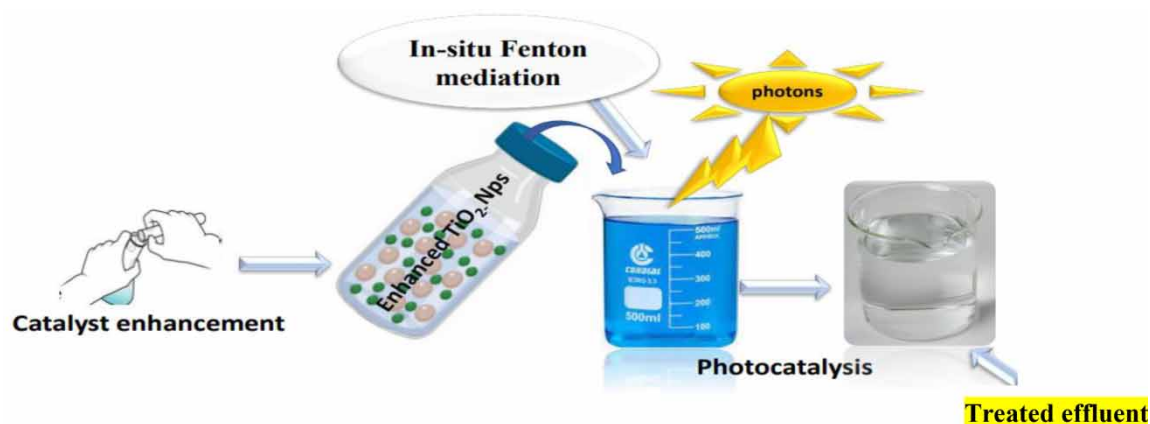
Effluents resulting from the frequent use of industrial azo dyes in textile operations have posed great toxicological impacts on man and the environment. The limitations of conventional treatment infrastructure necessitate the use of rapid Fenton-mediated catalytic systematic process to tackle the attendant treatment limitations. The study applied *in situ* Fenton-mediation process with constructed low power UV-LED reactor for rapid catalytic treatment of dye-laden effluent using enhanced acid and alkali TiO<sub>2</sub>-nanoparticles (Nps) (1–5%, i.e. 1–5 M) at definite experimental conditions, respectively. A comprehensive instrumental study was done to access the morphological, functional and elemental constituents of these nanocatalysts. The performance of the respective catalyst was evaluated using methylene blue (MB) dye at definite experimental conditions of pH, dosage, concentration and irradiation time. The results revealed a mesoporous structural nanocatalyst with increasing surface area after enhanced modification. The optimal experimental conditions of pH and concentration were recorded as 5 and 10 mg/L, respectively; while the most efficient nanocatalyst was 3 wt% alkali-modified TiO<sub>2</sub> (3% Ak-TiO<sub>2</sub>) having a degradation efficiency of 89.15% at 90 min of irradiation using 50 mg dosage in contrast to higher irradiation time and catalyst dosage for other catalysts.

**Key words:** degradation, Fenton-mediation, nanocatalyst, performance, photocatalysis, photon

### HIGHLIGHTS

- Development of rapid photocatalytic treatment process with built low-powered UV-LED reactor.
- Use of unique Fenton reagents and *in situ* mediation for effective dye degradation.
- Unique morphological enhancement of nanocatalyst for more effective degradation.

### GRAPHICAL ABSTRACT



## 1. INTRODUCTION

The evolution of textile industries and the increasing demands on the use of synthetic dyes corresponds to the generation of a large volume of textile effluent consisting of 10–30% of loosed dyes (Sarmah & Kumar 2011; Al-Rubaie & Mhessn 2012). Among the industrial dyes commonly used are the azo dyes (N=N). This category of dye takes a significant use of 70% among other dyes commercially (Oyetade *et al.* 2022). The industrial attention is based on their vast use in dyeing, printing, pigmentation and extensively in medicine and food colorants (Ameen *et al.* 2011; Kumar & Pandey 2018). Although they are less toxic and chemically stable in raw form, the indiscriminate discharge of their corresponding effluents is deleterious to human health and the environment at large (Kaur & Singhal 2014; Abayomi *et al.* 2020; Deriase *et al.* 2021; Oyetade *et al.* 2023). Treatment technologies categorized as physical, biological and chemical treatments have been applied for the remediation of recalcitrant dye pollutants (Xu *et al.* 2010; Kumar & Pandey 2018). However, the recalcitrant nature and chemo-transformative behavior of the dye molecules in textile wastewater remain challenging (Oyetade *et al.* 2022). In recent times, studies have focused on the use of photocatalysis as an efficient treatment technology to completely mineralize the selected recalcitrant dye pollutants (Xu *et al.* 2010; Zhu *et al.* 2010). Generally, the photocatalytic approach is a photon-induced process occurring which takes place at the surface of photon excited nanocatalysts, such as TiO<sub>2</sub>, ZnO h-BN, GO, SnO<sub>2</sub>, ZrO<sub>2</sub>, ZnO, CdS, Fe<sub>2</sub>O<sub>3</sub>, and so on (Hou *et al.* 2018). The mechanism involves the capturing of photon energy from light by the photocatalyst, excitation of the electrons from the valence band (VB) to the conduction band (CB) (electron-hole pair), formation of oxidizing and reducing sites, generation of radical species ( $\cdot\text{OH}$ ,  $\cdot\text{O}^{2-}$  and  $\cdot\text{OOH}$ ) and radical attack which mineralizes the dye molecules (Lopes Colpani *et al.* 2019). The radical attack leads to the degradation of dye molecules into CO<sub>2</sub>, H<sub>2</sub>O and other harmless substances (Sarmah & Kumar 2011; Hossain *et al.* 2020). Among the wide spectrum of photocatalysts semiconductors used, the selection of titanium dioxide (TiO<sub>2</sub>) is based on its cost-effectiveness, nontoxicity, biocompatibility, stability, possibility of recovery and reuse, corrosion resistance, flexibility in synthesis and surface modification with good adsorption-desorption rate (Haider *et al.* 2019). Furthermore, the semiconductor has high surface activity and excellent dye mineralization potential based on its unique oxidizing capacity (Jangid *et al.* 2021). This semiconductor generally exists as anatase, rutile and brookite, although other forms of TiO<sub>2</sub> are hollandite, columbite and ramsdellite which are generally unstable (Haider *et al.* 2019). Among the existing forms, rutile and anatase have the most appreciable use with known synthetic pathways such as the sol-gel method, hydrothermal, microemulsion and micelles, pulse laser deposition, and so on (Mezni *et al.* 2017). The vast applicability of rutile and anatase is based on its high oxidative power, photochemical stability, excellent potential energy of photogenerated electrons and appreciable photocatalytic activity (Macwan *et al.* 2011; Xia *et al.* 2014). However, the challenges of agglomeration of the nanoparticles (Nps), low reaction kinetics, insensitivity to visible light, frequent electron-hole recombination and low sorption properties resulted in the need for simultaneous enhancement of the performance via modification of the surface morphology and application of *in situ* Fenton-mediation for the process (Hou *et al.* 2018; Qutub *et al.* 2022; Oyetade *et al.* 2022; Zhang *et al.* 2021a, 2021b). The incorporation of Fenton-mediation in photocatalysis is based on its ability to generate or increase the availability of more radicals at the catalyst surface via the combination reaction of Fe<sup>2+</sup> and H<sub>2</sub>O<sub>2</sub> under acidic conditions. This action incredibly enhances capturing of photons from UV light and solar light via its association with a modified photocatalyst and the generation of more HO $\cdot$  to initiate an effective dye-radical attack (Li *et al.* 2020; Zhang *et al.* 2021a, 2021b). Hence, this study comparatively investigates the performance of *in situ* mediated photocatalytic degradation of methylene blue (MB) dye with acid- and alkali-enhanced TiO<sub>2</sub>-Nps and statistical optimization of the most efficient catalyst for industrial scale-up.

## 2. MATERIALS

### 2.1. Chemicals, instruments and glassware

High purity grade (99.5%) titanium dioxide (P25) powder consisting of mixed anatase and rutile phase was purchased at LOBA Chemicals in India. Other reagents such as HCl (37% v/v), H<sub>2</sub>SO<sub>4</sub> (97% v/v), anhydrous FeCl<sub>3</sub>, H<sub>2</sub>O<sub>2</sub> (30% v/v), NaOH and methylene blue dye MB (C<sub>16</sub>H<sub>18</sub>ClN<sub>3</sub>S) purchased from the same location were analytical grade. Furthermore, de-ionized water was used throughout the experiment, while other glassware and equipment such as a centrifuge machine, analytical weighing balance and oven were procured at the Nelson Mandela African Institution of Science and Technology (NM-AIST), Tanzania. A low power rating (18 W) UV-LED reactor was constructed at Arusha Technical College (ATC) in Tanzania with a power rating of 18 W.

## 2.2. Preparation of enhanced TiO<sub>2</sub>-Nps

Acid enhancement of the nanocatalyst (TiO<sub>2</sub>) was carried out according to the modified method reported by Park & Shin (2014) and Hou *et al.* (2018). This involved weighing 1.5 g of TiO<sub>2</sub> into 100 mL of 0, 1, 2, 3, 4 and 5 mol dm<sup>-3</sup> concentrations of H<sub>2</sub>SO<sub>4</sub> (AC-TiO<sub>2</sub>), with stirring for 3 h. The solution was then centrifuged at 3,000 rpm, filtered and washed with ultrapure water three times before drying at 105 °C in the oven for 2 h. The resulting material was calcinated at 450 °C for 2 h to eliminate water trappings in the catalyst matrix and pulverized to obtain powdered material. Each sample was labeled appropriately 0% (untreated TiO<sub>2</sub>-Nps) and then 1–5% (i.e. 1–5 M), respectively. The procedure was repeated using NaOH to obtain alkali-modified TiO<sub>2</sub>-Nps (AK-TiO<sub>2</sub>).

## 2.3. Nanocatalyst characterization

The morphological properties of prepared samples were analyzed using a Zeiss Ultra Plus 55 Field Emission Scanning Electron Microscope (FE-SEM) at 2.0 KV acceleration potential with energy-dispersive X-ray spectroscopy (EDX). N<sub>2</sub> adsorption-desorption isotherms of the samples were achieved through the aid of a micromeritics TriStar II 3020 device run at a relative pressure ( $P/P_0$ ) ranging from 0.01 to 1.0 with the samples being pre-degassed at a temperature of 120 °C for 16 h in a vacuum before the analysis was performed. A Brunauer–Emmett–Teller (BET) and Barrett–Joyner–Halenda (BJH) model was adopted to estimate the samples' surface area and pore size distribution (PSD), respectively. X-ray diffraction (XRD) patterns of the samples were recorded on a Bruker D8 Advance X-ray diffractometer with Cu K $\alpha$  radiation. The Fourier-transform infrared spectra (FT-IR) of the samples were recorded on a Vertex 70 spectrometer in a range from 4,000 to 400 cm<sup>-1</sup>. The initial and final concentrations of the treated effluent were quantified as a function of the absorbance using UV-Vis diffuse reflectance spectroscopy (UV-vis DRS; Shimadzu 2600, Kyoto, Japan).

## 2.4. Photocatalytic performance evaluation

Performance evaluation of the photodegradation of the dye molecules (MB) in aqueous solution via the simultaneous use of catalyst with *in situ* Fenton-mediation was studied under constructed cost-effective low-powered UV-LED reactor. Aqueous suspension of MB effluent (100 mL, 10 mg/L) was placed in a 250 mL beaker and a measured amount of the TiO<sub>2</sub>-Nps was added. Before irradiation, the suspensions were magnetically stirred in the dark for approximately 60 min. Constant stirring of the suspensions was maintained before and during the irradiation of UV light (Shahabuddin *et al.* 2018). A unique Fenton reagent involving the anhydrous FeCl<sub>3</sub> and H<sub>2</sub>O<sub>2</sub> was prepared via the modified method of Liu *et al.* (2019) and added *in situ* to the process before irradiation. At a definite time interval, 5 mL of the aliquot was taken and centrifuged at 3,000 rpm. The supernatant was quantified using the UV-Vis at a predetermined  $\lambda_{\max}$  of 666 for the MB. Equation (1) was used to determine the degradation efficiency. The same process was carried out for acid (AC-TiO<sub>2</sub>) and alkali-modified (AK-TiO<sub>2</sub>) nanocatalysts at 50, 70, 90 and 110 mg dosages, respectively. The procedure was repeated at the pH range of 3–11, a concentration of 10–40 and an irradiation time of 15–90 min at 50 mg/100 mL of the aqueous solution

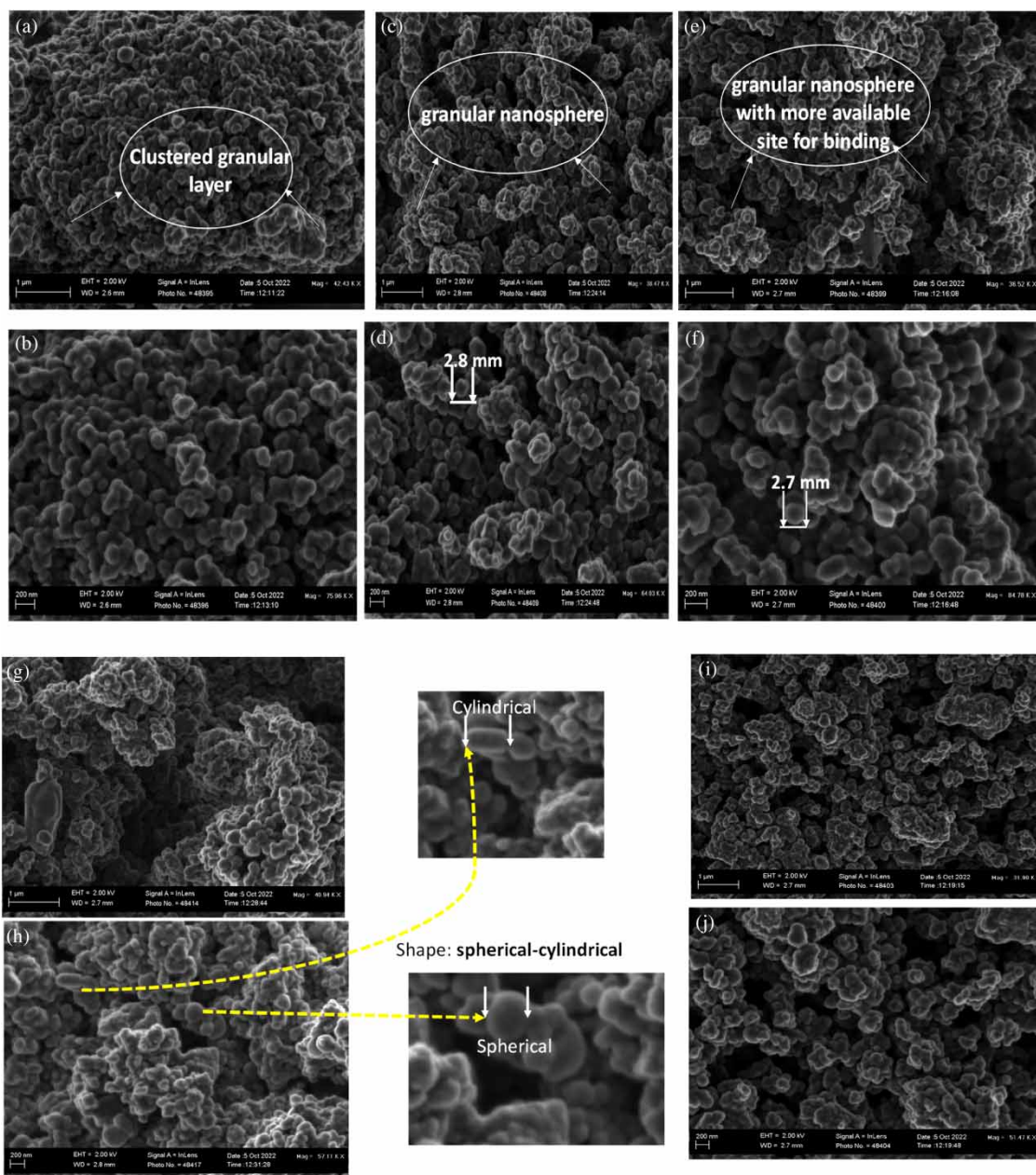
$$\% \text{Degradation efficiency} = \frac{C_0 - C_t}{C_0} \times 100 \quad (1)$$

where  $C_t$  is the concentration at time  $t$ ,  $C_0$  initial dye concentration

## 3. RESULTS AND DISCUSSION

### 3.1. Morphological characterization of nanocatalysts

The FE-SEM image in Figure 1(a) and 1(b) describes the morphological arrangement of the untreated P25 TiO<sub>2</sub>-Nps catalyst, Figure 1(c) and 1(d) depicts the 3% acid and alkali-enhanced catalyst while Figure 1(g)–1(j) shows a 5% enhanced catalyst at different magnifications. From the imaging, a highly stacked and clustered morphological arrangement was observed for untreated TiO<sub>2</sub>-Nps in Figure 1(a) and 1(b) and for all the acid-enhanced catalysts. The clustered morphology from the imaging was equally reported by Kumar & Pandey (2018), which is connected with lower binding sites available and undesirable agglomeration. From Figure 1, the structural expression of the catalyst is a spherical cylindrical nanocatalyst with an average diameter of 2.8 nm. These structural features agree with the FE-SEM studied by Sarmah & Kumar (2011) and Zhou *et al.* (2022) on TiO<sub>2</sub>-Nps; however, Hou *et al.* (2018) added that the clustered morphological characteristics of the TiO<sub>2</sub>-Nps and the acid-enhanced catalyst are often responsible for the agglomeration phenomenon which lowers the photocatalytic

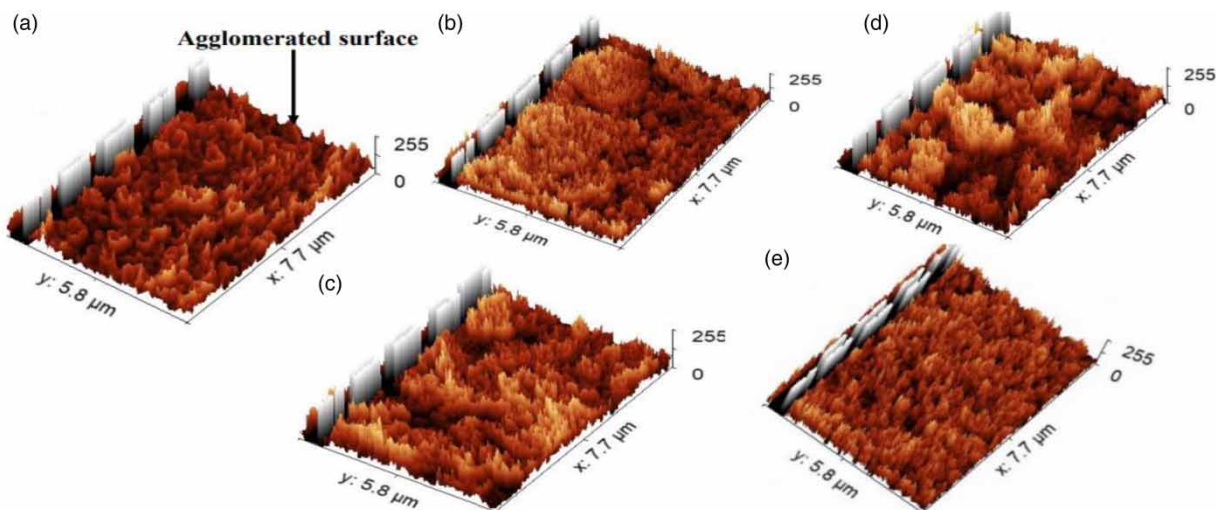


**Figure 1** | FE-SEM of (a,b)  $\text{TiO}_2$ -Nps with 3% AC- $\text{TiO}_2$  (c,d); 3% AK- $\text{TiO}_2$  (e,f); 5% AC- $\text{TiO}_2$  (g,h); 5% AK- $\text{TiO}_2$  (i,j) with their structure.

performance. Also, the cylindrical morphological shape suggests its unique advantage and use as support in the formation of composite via *in situ* polymerization with macromolecules (Zhu *et al.* 2010; Wahyuni *et al.* 2018; Jangid *et al.* 2021). The modification of the surface morphology of synthesized catalysts may facilitate more interparticle spacing and surface growth, thus increasing the availability of active sites for catalyst-adsorbent binding (Zare *et al.* 2018; Lee & Patel 2022; Oye-tade *et al.* 2022). The impacts of the treatment, respectively are revealed in terms of the displayed surface growth topology  $\text{TiO}_2$ -Nps in Figure 2. It is necessary to add that the rutile and the anatase components of  $\text{TiO}_2$ -Nps are structurally cylindrical as equally exhibited from the imaging in Figure 3 (Hou *et al.* 2018; Haider *et al.* 2019).

### 3.2. BET analysis

The pattern of the BET adsorption-desorption isotherm in Figure 3(a) and 3(b) structurally describes the features of the pure and enhanced catalyst. The results showcase a typical type IV hysteresis loop of  $\text{N}_2$  adsorption-desorption isotherm for all



**Figure 2** | 3D Surface imaging of  $\text{TiO}_2$  (a); (b,c) 3% and (c–e) 5% AC- $\text{TiO}_2$  and AK- $\text{TiO}_2$ .

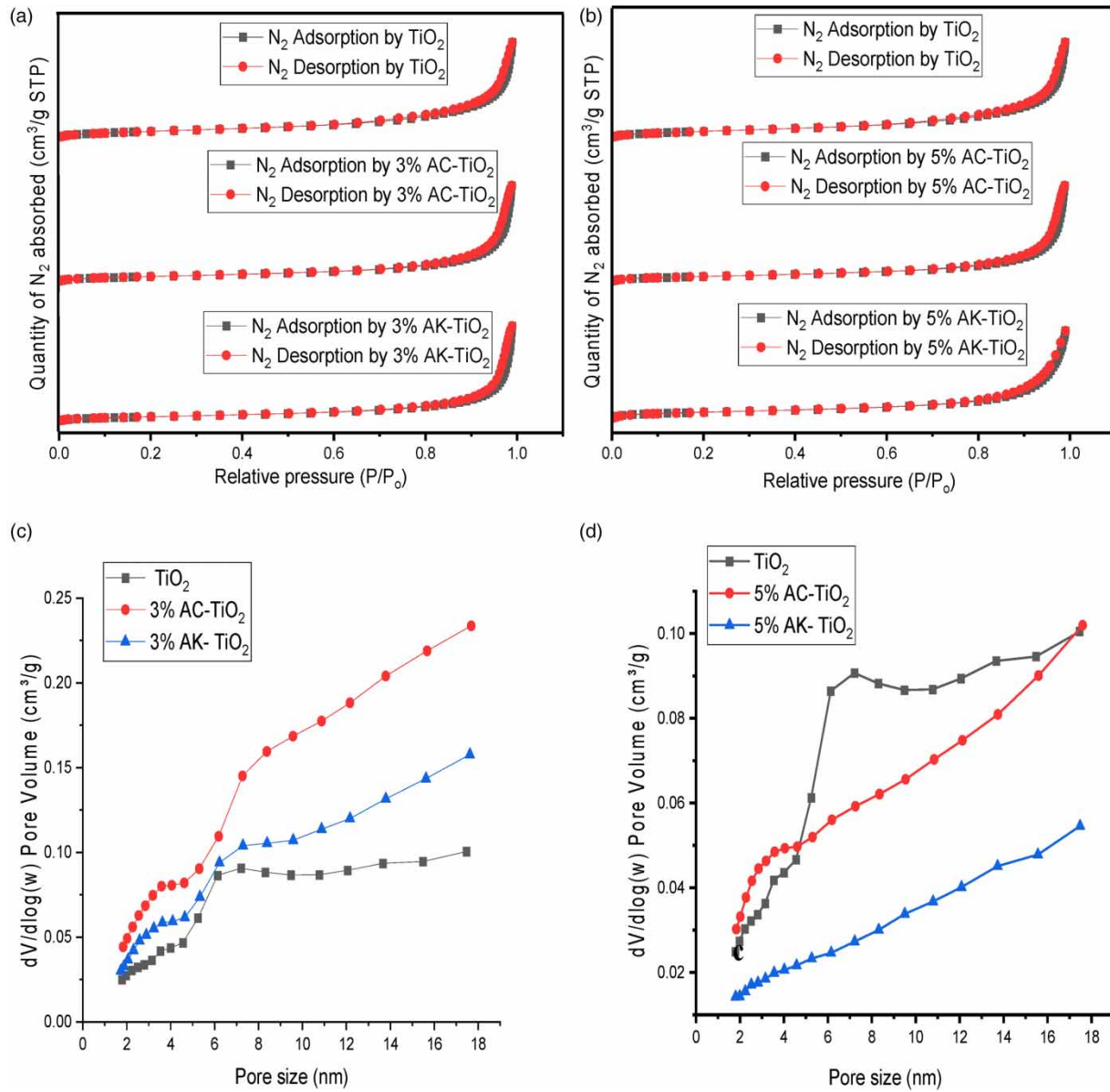
samples, indicating well-developed mesopores (Carja *et al.* 2001; Xiang *et al.* 2010). This report agrees with a similar observation on the mesoporous structure of  $\text{TiO}_2$ -Nps made by Kumar & Pandey (2018), Liu *et al.* (2019), and Wahyuni *et al.* (2018). From the results, the significant increase in the quantity adsorbed set in at  $P/P_0$  region  $> 0.8$ . At this point and beyond, more opening of the hysteresis loop was observed which accounts for stronger multilayer adsorption (Nie *et al.* 2013). Furthermore, the vital features of a specific area, pore diameter and pore volume are described in Table 1, while Figure 3(c) and 3(d) comparatively shows the pore size of 3 and 5% enhanced  $\text{TiO}_2$ -Nps with its acid and alkali, respectively. From Table 1, the lowest pore size observed was 14.33 nm similar to the 14.73 nm size reported by Hou *et al.* (2018). However, the value increases significantly after respective acid and alkali treatment. This action was similar to the BET surface areas of 47.97 for untreated, while the highest was  $91.82 \text{ m}^2\text{g}^{-1}$  for 3% acid modification followed by  $64.74 \text{ m}^2\text{g}^{-1}$  for 3% alkali modification, respectively. The tunability of the morphological properties increased the surface area of the catalyst, facilitating the prompt electron transport dynamics and high ion diffusion, allowing improved photochemical performance (Carja *et al.* 2001; Mezni *et al.* 2017; Kumar & Pandey 2018).

### 3.3. XRD analysis

XRD patterns of pure  $\text{TiO}_2$ -Nps, 3% (Figure 4(a)) and 5% (Figure 4(b)) acid and alkali-enhanced catalysts were, respectively, reported. Figure 4 shows the patterns for pure anatase  $\text{TiO}_2$ -Nps, at  $25^\circ$ ,  $38^\circ$ ,  $48^\circ$ ,  $55.1^\circ$  and  $63.2^\circ$  which correspond to (101), (103), (200), (211) and (204) planes of  $\text{TiO}_2$ . However, the structural patterns at the plane (110) correspond to the rutile structure (JCPDS No. 21-1272) (Ananpattarachai *et al.* 2009; Moon *et al.* 2011). The observed features are in agreement with the high purity grade P25  $\text{TiO}_2$  used by Plermjai *et al.* (2019); however, lower than those reported of  $\text{TiO}_2$  synthesized via the sol-gel method. From Figure 4(a) and 4(b), it was observed that the intensity of the peaks decreases significantly after the acid and alkali modification process. Furthermore, the higher the intensity of the peaks the more crystalline the arrangement of the Nps, while the decrease in peak intensity suggests the transformation of the surface morphology of the Nps to an amorphous state (Xia *et al.* 2014; Hou *et al.* 2018; López-López *et al.* 2022). This morphological transformation justifies the observed increasing BET surface area and pore volume in Table 1.

### 3.4. FT-IR analysis

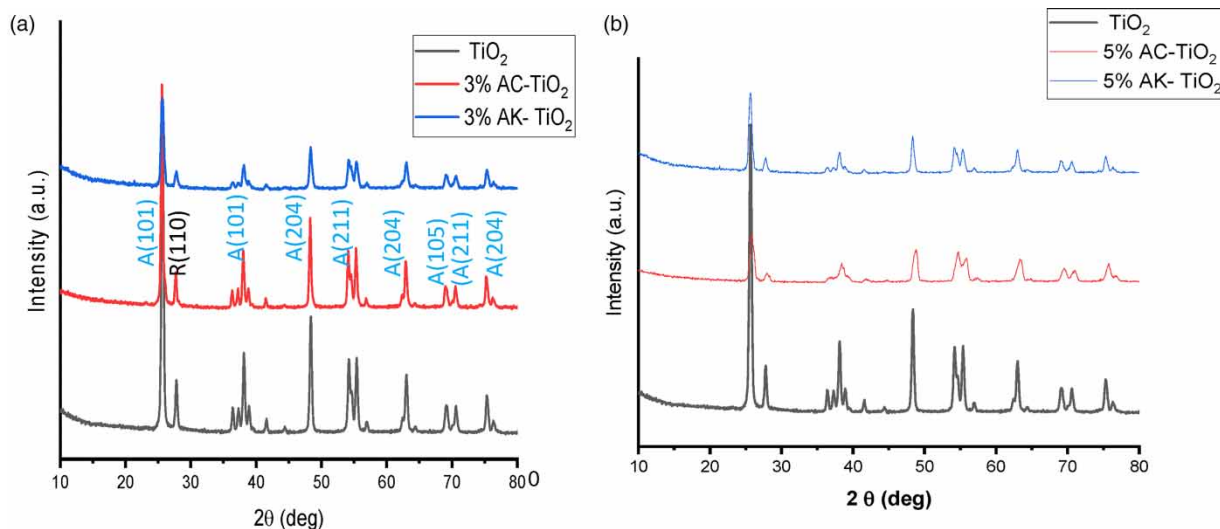
Figure 5 shows the FT-IR spectra of the nanocatalyst with 3% (Figure 8(a)) and 5% (Figure 8(b)) acid- and alkali-enhanced nanocatalyst, respectively. From the spectra, the peak intensity around  $400\text{--}800 \text{ cm}^{-1}$  reveals the functional characteristic of the metal oxide bond (Ti–O bond), while the peak at  $1,400 \text{ cm}^{-1}$  shows stretching vibrations of Ti–O–Ti (Wang *et al.* 2015; Hou *et al.* 2017). The functional features at this region may facilitate the dye-adsorbent coordination in adsorption which enhances the improved photocatalytic performance of the nanomaterial (Abebe *et al.* 2020). Also in Figure 5, the bend of O–H observed at  $3,454.51 \text{ cm}^{-1}$  is often assigned to the OH free radical associated with hydrogen bond



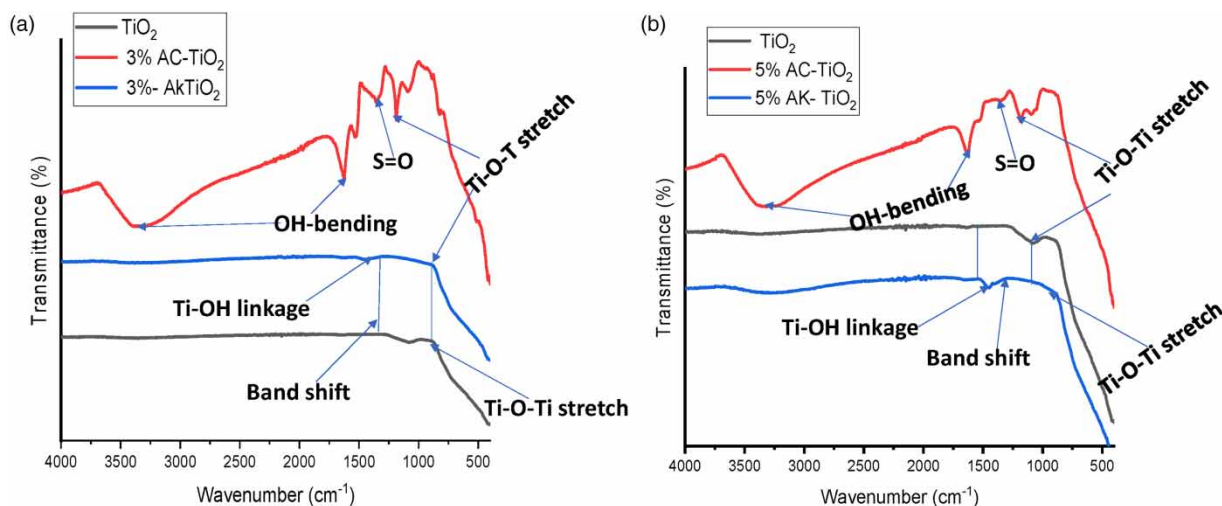
**Figure 3** | BET adsorption–desorption isotherm of 3% (a) and 5% (b) and pore size distribution of TiO<sub>2</sub>-Nps with enhanced nanocatalyst of 3% (c) and 5% (d) of TiO<sub>2</sub>-Nps with enhanced nanocatalyst.

**Table 1** | Physicochemical properties of the samples

S/N	Samples	BET surface area (m <sup>2</sup> g <sup>-1</sup> )	Pore volume (cm <sup>3</sup> /g)	Pore size (nm)
1	TiO <sub>2</sub>	47.9654	0.17	14.22
2	3% AC-T	91.8267	0.42	18.33
3	5% AC-T	60.5754	0.32	21.28
4	3% AK-T	64.7434	0.30	18.37
5	5% AK-T	50.3858	0.21	16.64



**Figure 4** | XRD pattern of TiO<sub>2</sub>-Nps with enhanced nanocatalyst of 3% (a) and 5% (b).



**Figure 5** | FT-IR spectra of TiO<sub>2</sub>-Nps with enhanced nanocatalyst of 3% (a) and 5% (b).

(Ahmadizadegan 2017; Martakov *et al.* 2018). Additionally, an observed band shift in Figure 5(a) and 5(b) could significantly contribute to the dye coordination and radical formation at the dye-catalyst interphase which improves the catalyst efficiency (Lu & Astruc 2020). The peak at 1,417 cm<sup>-1</sup> corresponds to the S = O linkage on the acid-enhanced catalyst with increasing intensity at 5%. This band shows the presence of sulfate ions which may act as radical scavengers to lower the generation of hydroxyl radicals during photocatalysis (Park & Shin 2014). Generally, the FT-IR spectra band of photocatalyst interprets the functionality of the material and the bond existing within the atoms, and these forecast the expected reaction mechanism and rate of reaction (Shahabuddin *et al.* 2018; Abebe *et al.* 2020; Oyetade *et al.* 2022).

### 3.5. EDX analysis

The elemental composition and the percentage abundance are described in Table 2. Table 2 reveals that the predominant elemental composition of Ti (29.91%), O<sub>2</sub> (47.74%) and Si (22.35%) were present in the pure TiO<sub>2</sub>-Nps which agrees with the observed functional features of the FT-IR spectra band in Figure 5. However, with alkaline modification the percentage abundance of Ti increases to 54.46 and 59.63% in 3 and 5% acid modification, respectively. On the other hand, the highest



**Table 2** | EDX elemental composition

S/N	Samples	Percentage elemental composition (%)						
		Ti	O	Na	Si	Cl	S	Al
1	TiO <sub>2</sub>	29.91	47.74	–	22.35	–	–	–
2	3% AC-T	54.46	43.24	–	1.86	–	0.44	–
3	5% AC-T	59.63	37.69	–	2.22	–	0.47	–
4	3% AK-T	58.96	38.98	0.77	0.44	0.64	–	0.22
5	5% Ak-T	59.26	39.01	0.79	0.20	0.74	–	–

titanium composition quantified after alkali treatment was 58.96 and 59.26% for 3 and 5% alkali modification, respectively. The sulfur content of 1.86 and 2.22% in 3% AC-TiO<sub>2</sub> and 5% AC-TiO<sub>2</sub> can be attributed to the sulfuric acid treatment while the presence of Na can be attributed to the NaOH treatment of the Nps. It is necessary to add the increase in element composition of titanium to the treatment completely remediate the silicon content of the TiO<sub>2</sub>-Nps which could influence the band gap features and the performance of the semiconductor during adsorption and photocatalysis (Martakov *et al.* 2018; Lu & Astruc 2020). Hence, the higher the amount of titanium and oxygen elements present, the more the possibility of effective coordination and bond establishment needed to adsorb dye molecules before photocatalysis (Angkaew & Limsuwan 2012).

### 3.6. Photocatalytic activities and effects of independent parameters

#### a. Performance test of enhanced TiO<sub>2</sub> nanocatalyst

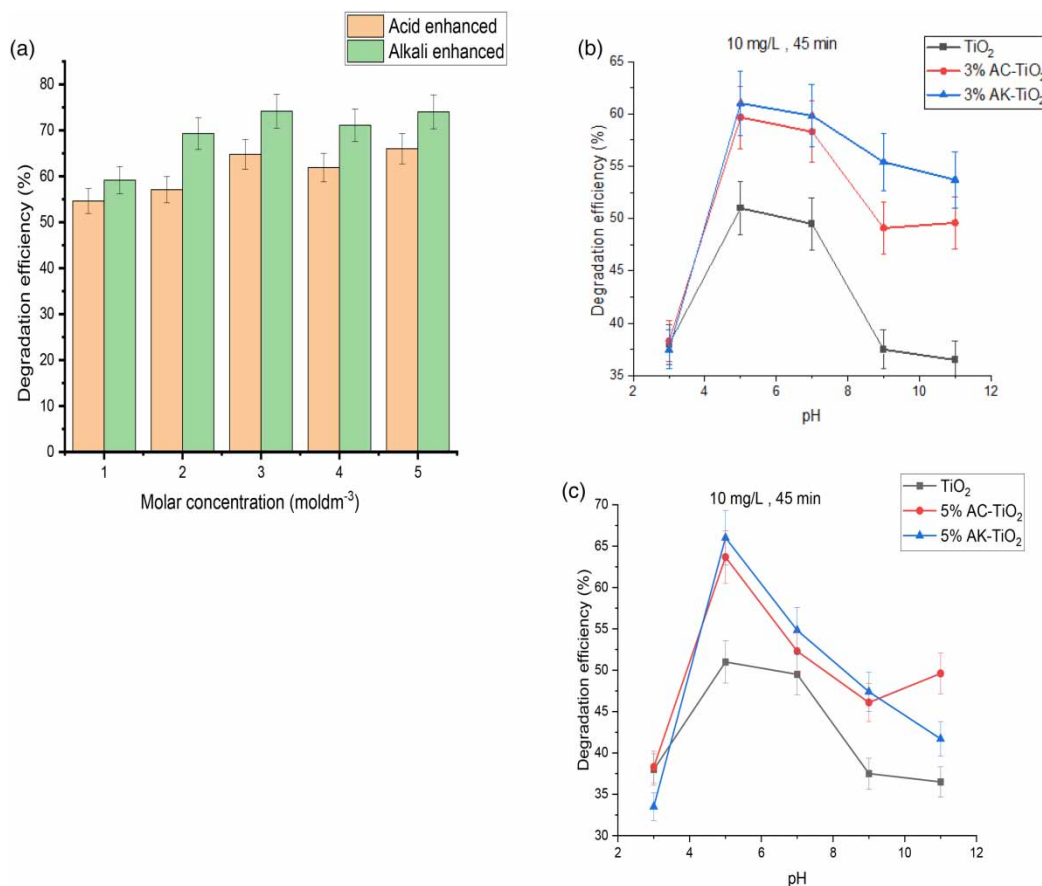
The results in Figure 6(a) evaluated the preliminary performance of Fenton-mediated TiO<sub>2</sub>-Nps enhanced with 1–5 M concentration of H<sub>2</sub>SO<sub>4</sub> and NaOH, respectively. The result reveals the minimal performance of 54.6 and 59.14% for acid- and alkali-enhanced nanocatalysts. However, the optimal performance recorded was at 3 M (64.78 and 74.15%) and (60.1 and 74.03%) 5 M, respectively, for acid- and alkali-enhanced nanocatalysts.

A similar performance was recorded by Hou *et al.* (2018), however, at a considerably higher concentration of 10 M NaOH. Furthermore, Park & Shin (2014) added that although the acid treatments of TiO<sub>2</sub> nanoparticle yield hydroxyl and increase the hydrophilicity of the catalyst, the presence of SO<sub>4</sub><sup>2-</sup> from the H<sub>2</sub>SO<sub>4</sub>-treated catalyst at some point acts as •OH scavenger which prevents the photocatalytic process. However, it is necessary to add that the *in situ* Fenton-mediation during the process may account for the appreciable dye photodegradation, especially at 3 and 5 M concentrations of acid. The use of Fenton-mediation facilitates the generation of a significant amount of desired •OH which promotes decolourization of dye molecules adsorbed onto the surface of the modified nanocatalyst (Yasar & Yousaf 2012; Zhang *et al.* 2021a, 2021b).

#### b. Effect of pH on photocatalysis

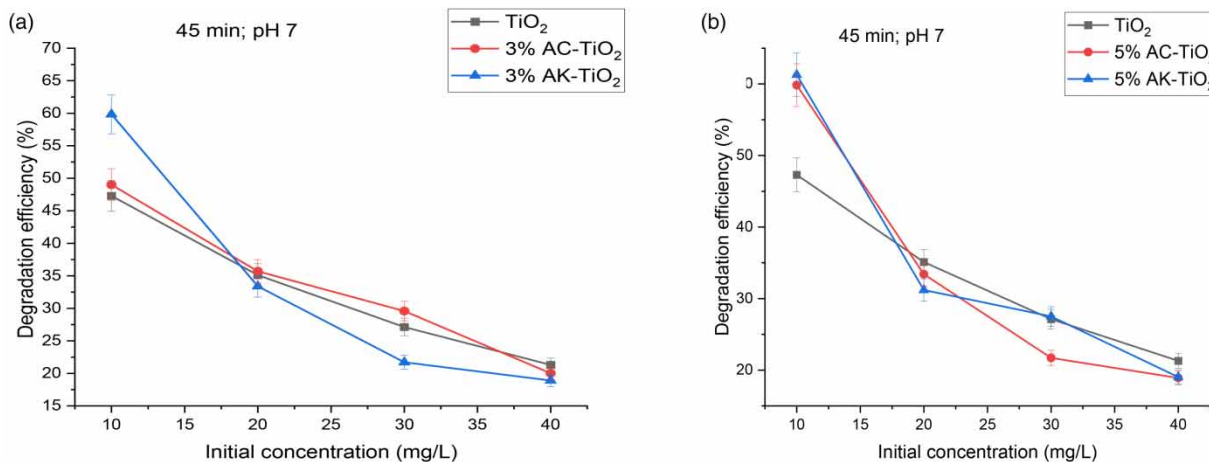
Figure 6(b) and 6(c) shows the effect of varying pH (3–11) for the Fenton-mediated photocatalytic process using the most efficient acid- and alkali-enhanced catalysts in Figure 6(a). From the results, the optimal pH value of 5 was recorded with degradation efficiency of 51, 59.67, 61.02, 63.67 and 66.02%, respectively, for pure, 3 and 5 M acid- and alkali-enhanced photocatalysts at 45 min. Abdellah *et al.* (2018) suggested that the basic nature of MB and its interaction with and amphoteric catalyst (TiO<sub>2</sub>-Nps) accounts for a desired slightly acidic pH (<5.8) which builds up a positively charged surface to establish electrostatic interaction with the dye molecules. Furthermore, the result of the optimal pH of 5 agrees with the study carried out by Jangid *et al.* (2021) and Shahabuddin *et al.* (2018) using MB as a model dye. The higher performance at this pH is because the positive surface of TiO<sub>2</sub>-Nps in an acidic medium facilitates the hydroxyl ion generation needed to form radicals (Jiménez *et al.* 2015). Additionally, the OH• concentration increases with the increasing presence of •OH ions due to the H<sup>+</sup> ions in the acidic medium (Ma *et al.* 2014). Also, the formation of electrostatic interaction between the catalyst and dyes in the effluent and radical generation depend on the pH of the medium (Dresselhaus *et al.* 2018). It is necessary to add that the natural and synthetic dyes are generally called either cationic, anionic or neutral. Thus, the nature of the dye constitutes to its reactivity in effluents and suggests optimal pH for its remediation (Joshi & Shrivastava 2012; Abdellah *et al.* 2018).

#### c. Effect of initial concentration on photocatalysis



**Figure 6** | Preliminary performance test of enhanced TiO<sub>2</sub>-Nps at 10 mg/L (a); 1 g/L and 45 min; effect of pH on degradation efficiency of 3% (b) and 5% (c) enhanced TiO<sub>2</sub>-Nps.

The effect of initial concentration on the Fenton-mediated process was studied at different concentrations ranging from 10 to 40 mg/L with 50 mg catalyst dosage and 45 min light UV irradiation. Figure 7(a) and 7(b) shows significant reduction with increasing concentration up to 40 mg/L, although we noted optimal concentration of 10 mg/L for the process. Similar optimal concentration was reported by Marziyeh *et al.* (2012), Jangid *et al.* (2021) and Mpelane *et al.* (2020) for MB dye using the



**Figure 7** | Effect of initial concentration on degradation efficiency of for 3% (a) and 5% (b) enhanced TiO<sub>2</sub>-Nps.

nanocatalyst and with other materials forming composites. The descending plot in Figure 7(a) and 7(b) showcases possible covering and oversaturation of the active sites of the catalyst which reduces dye–photocatalyst interaction. Hence, it lowers the generation of free radicals which enhances dye degradation due to the accessibility of photon energy to the active sites (Marziyeh *et al.* 2012; Dutta *et al.* 2021; Oyetade *et al.* 2022).

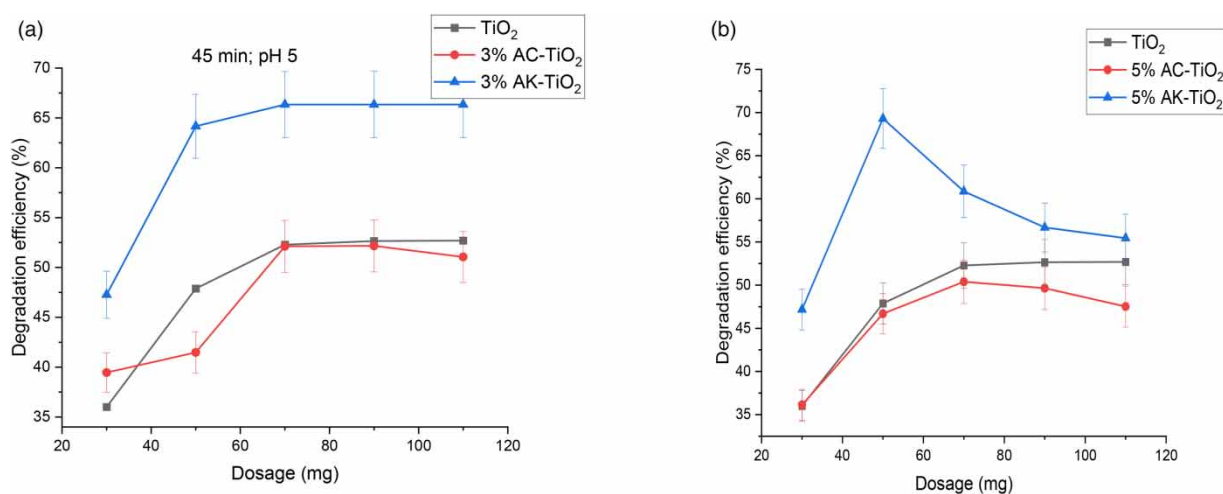
#### d. Effect of dosage on photocatalysis

The effect of dosage generally accounts for the reactive performance of the catalyst and its economic implication. Figure 8 reveals the degradation efficiency at different catalyst dosage (30–110 mg) under 45 min UV irradiation, optimum pH (5) and initial concentration of 10 mg/L, respectively. From the results, the optimum dosage ascribed to the pure TiO<sub>2</sub>-Nps was 70 mg which slightly increases to 90 mg. However, 50 mg optimal dosage was recorded for 3 and 5 M alkali-enhanced TiO<sub>2</sub>-Nps in contrast to 70 mg optimal dosage for acid-enhanced TiO<sub>2</sub>-Nps. Beyond this optimal point, there is a level of constancy followed by a gradual decline in performance. From the result, the alkali-enhanced catalyst has an efficiency of 69.3% at 50 mg, compared to 52.65 and 66.34% degradation at 70 and 90 mg for pure TiO<sub>2</sub>-Nps and acid-enhanced TiO<sub>2</sub> (AC-TiO<sub>2</sub>-Nps).

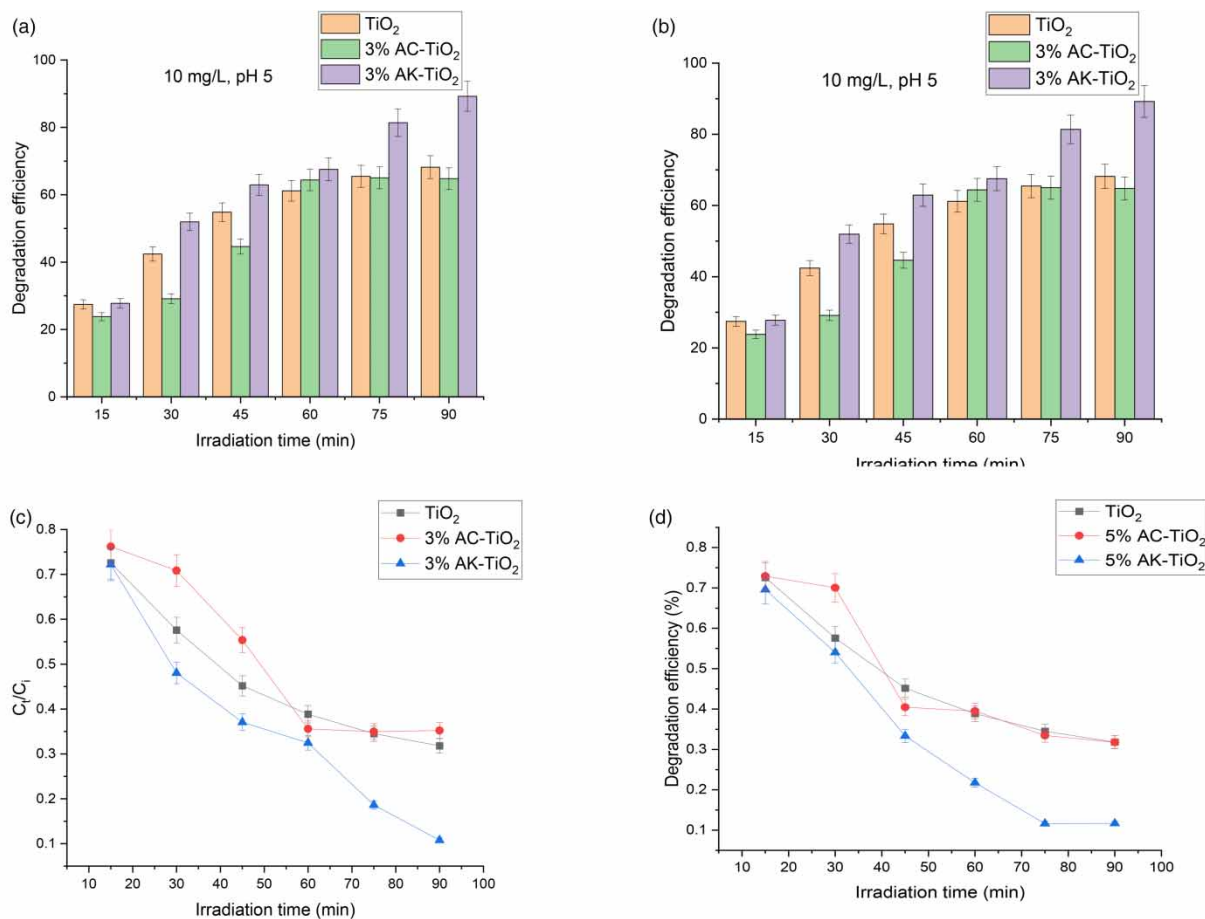
The increase in photodegradation is due to the increasing amount of sites available for binding which results in the formation of more active radicals (hydroxyl and superoxide) that initiate the degradation reaction (Suttiponparnit *et al.* 2011; Abdellah *et al.* 2018). Although high catalyst loading of TiO<sub>2</sub> particles impedes incident UV irradiation apart from the possibility of agglomeration owing to clustered surface area (Wang *et al.* 2010; Saleh & Gupta 2012; Abdellah *et al.* 2018). Therefore, beyond the optimal dosage, coupled with a low surface area of the catalyst, reduction in decolorization efficiency is set in, although a similar optimal dosage was recorded by Hou *et al.* (2018) for alkali-enhanced TiO<sub>2</sub> (AK-TiO<sub>2</sub>-Nps). On the other hand, Park & Shin (2014) uses 500 mg of acid-enhanced TiO<sub>2</sub> for optimal dye photocatalysis. The significant efficiency of the AK-TiO<sub>2</sub>-Nps catalyst is due to the increase in the surface area and lowered agglomeration as revealed by the BET, SEM and 3D surface image, while the saturation and eventual agglomeration with increasing dosages accounts for the gradual reduction of the process (Chatterjee *et al.* 2017; Dutta *et al.* 2021; Bayuo *et al.* 2023). Hence, the surface modification of the nanocatalyst often enhances bonding activities such as electrostatic interactions, Van der Waals forces, hydrogen bonding and  $\pi$ - $\pi$  interactions which enhance the photocatalytic process, however, at optimal dosage to avoid agglomeration (Ma *et al.* 2014; Jiménez *et al.* 2015).

#### e. Effect of irradiation time on photocatalysis

The degradation efficiency of the Fenton-mediated photocatalysis of MB at varying irradiation times using pure and enhanced TiO<sub>2</sub>-Nps as described by Figure 9(a) and 9(b), while Figure 9(c) and 9(d) shows the degradation rate ( $C_t/C_0$ ) of MB dye over time. From the results, 71.48, 69.01 and 89.15% were recorded for TiO<sub>2</sub>, 3% AC-TiO<sub>2</sub> and 3% AK-TiO<sub>2</sub> (3 M), respectively. In contrast, 68.19 and 88.37% for 5% AC-TiO<sub>2</sub>, 5% AK-TiO<sub>2</sub> (5 M) were, respectively, quantified.



**Figure 8** | Effect of catalyst dosage on degradation efficiency for 3% (a) and 5% (b) enhanced TiO<sub>2</sub>-Nps.



**Figure 9** | Effect of irradiation time on (a,b) degradation efficiency and (c,d) degradation rate of MB.

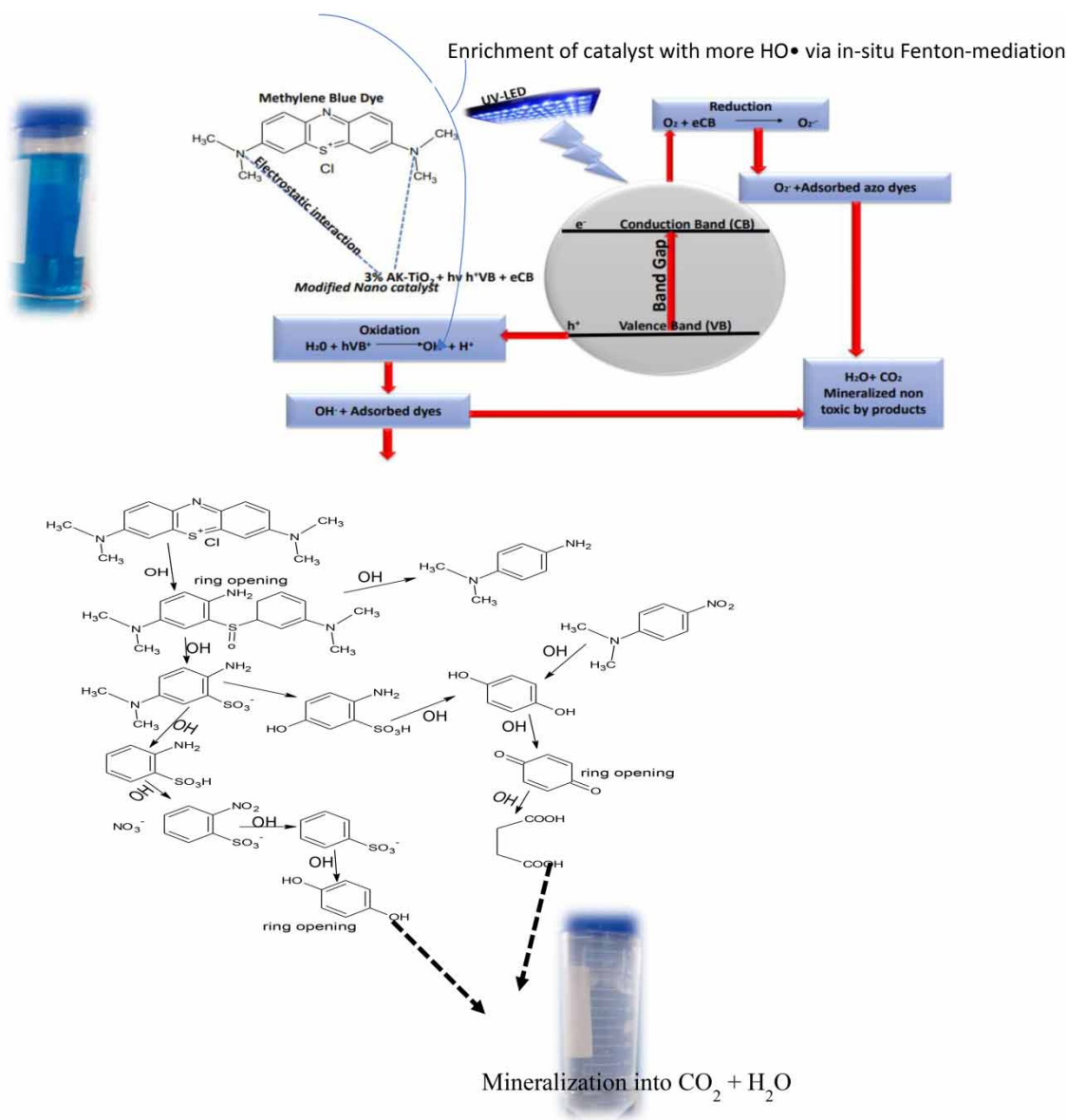
Although a similar amount of degradation was put forward by [Hou \*et al.\* \(2018\)](#) and [Kumar & Pandey \(2018\)](#) at a higher time range of 120 and 150 min. The lower time rate may be due to the novel application of *in situ* Fenton-mediation to improve the reaction rate of the process using an enhanced catalyst. This accounts for the high radical generation with lower recombination desirable to initiate the radical attack and eventual degradation ([Zhang \*et al.\* 2021a, 2021b](#)). Also, the adoption of *in situ* mediation improves the homogeneity of the solute–solvent interface while facilitating the efficient mass transfer and shorter reaction time ([Tunc Dede \*et al.\* 2019](#)). Although the Fenton-mediation is challenged with the generation of iron sludge, studies revealed that the use of the modified co-photocatalyst (TiO<sub>2</sub>-Nps) with the low concentration of iron in the Fenton reagent leads to the generation of little or no iron sludge ([Chacó \*et al.\* 2006](#); [Dong \*et al.\* 2020](#)). The use of this multiple process is called photo-Fenton where the electron generated by the co-photocatalyst is captured by Fe<sup>3+</sup> to produce Fe<sup>2+</sup> which combines again with H<sub>2</sub>O<sub>2</sub>, thereby preventing covering the surface of the catalyst leading to its deactivation ([Mokhbi \*et al.\* 2019](#); [Dong \*et al.\* 2020](#)).

Additionally, at an optimum time of 90 min, the lower degradation of acid-enhanced catalyst is due to the possibility of agglomeration as described from the SEM image and inhibition of radical attack as a result of sulfate ion acting as radical scavengers ([Abdellah \*et al.\* 2018](#); [Shahabuddin \*et al.\* 2018](#)). Furthermore, after the darkroom adsorption–desorption process, at 15 min irradiation, the lower degradation efficiency for all catalysts is due to the generation of fewer electron–hole pairs before radical formation and degradation of adsorbed dye molecules ([Jangid \*et al.\* 2021](#)). However, as time increases, the degradation efficiency increases, respectively. It is worthy of note that the highest efficiency of 89.15 and 88.97% for 3 and 5 M alkali-enhanced TiO<sub>2</sub> indicates the successful modification of the surface morphology as described by the SEM results which enrich the catalyst with significant binding sites and possibly influence its bandgap ([Ahmadizadegan 2017](#); [Debnath \*et al.\* 2021](#); [Oye-tade \*et al.\* 2022](#)). The process of bandgap tunability and surface modification in this regard limits the possibility of agglomeration and recombination of electron–hole pair ([Bingham & Daoud 2011](#); [Eskizeybek \*et al.\* 2012](#); [Jangid \*et al.\* 2021](#)). [Shahabuddin](#)

*et al.* (2018) added that the larger the surface areas the more active sites available for binding and the lower the agglomeration rate of the nanocomposite. However, the organic dye has light-absorbing potential and can undergo electronic transition via intersystem crossing leading to self-decomposition as the singlets and triplets species are formed (Subramanian *et al.* 2014; Shahabuddin *et al.* 2018). The formation of these species is enhanced by their interaction with photon-active and active site-enriched nanocatalyst which reacts with oxygen and water molecules to generate peroxide, superoxide and hydroxyl radicals. This process is facilitated at a lower time via Fenton-mediation (Shahabuddin *et al.* 2018; Oyetade *et al.* 2022).

### 3.8. Reaction mechanism

The surface modification via alkali modification is significant in charge separation during the photocatalytic process. The preliminary adsorption-desorption in a dark room establishes an electrostatic bond and enhances the adsorbent-adsorbate linkage between TiO<sub>2</sub>-Nps and MB dye (Figure 10). Irradiation of the system with UV-LED results in the excitation of electrons from the valance band to the CB with appreciable charge separation due to the preliminary alkali modification process.



**Figure 10** | Reaction mechanism.

Radicals such as hydroxyl radicals ( $\text{OH}\cdot$ ), superoxide radical anions ( $\text{O}\cdot^{2-}$ ) and hydroperoxyl radicals ( $\cdot\text{OOH}$ ) are generated during this process (Zangeneh *et al.* 2015; Qamar *et al.* 2019). Also at the optimal pH of 5 (slightly acidic condition), the surface of the amphoteric photocatalyst ( $\text{TiO}_2\text{-Nps}$ ) becomes positively charged, thereby establishing electrostatic reaction with the negatively charged model dye (MB), this process facilitates effective adsorption of the dye molecules unto the surface of the catalyst before the radical attack on irradiation (Jiménez *et al.* 2015; Abdellah *et al.* 2018). During the irradiation process, a spontaneous and simultaneous redox reaction alongside a radical attack of the adsorbed dye molecules occurs, leading to the preliminary opening of the ring as described in Figure 10. However, the *in situ* mediation of the process by Fenton reagents accounts for the generation of a larger amount of radical which combines with the radical generated by the action of the nanocatalyst in Equations (3)–(7). The reaction eventually terminates at the point of mineralization of the dye molecules into  $\text{CO}_2$  and  $\text{H}_2\text{O}$  which is reflected in decolorization of the effluent in Figure 10 (Asghar *et al.* 2015; Jangid *et al.* 2021).



### 3.9. Comparison of degradation efficiency

The performance of the most effective enhanced  $\text{TiO}_2$  (3% AK- $\text{TiO}_2$ ) is compared with other reports at optimal experimental conditions for the degradation of MB in Table 3. From the comparative results, the use of *in situ* Fenton-mediated photocatalysis and enhanced catalyst (3% AK- $\text{TiO}_2$ ) shows appreciable efficiency in contrast to reagents such as rihodizonic acid and salicylic acid used apart from their reported toxicity and cost intensiveness. Furthermore, a lower amount of NaOH

**Table 3** | Comparison between the present study and reported  $\text{TiO}_2$ -enhanced catalyst for photodegradation of MB dye

Nanocatalyst	pH	Initial conc (mg/L)	Source	Catalyst dosage (mg)	Irradiation time (min)	Efficiency (%)	References
10 M NaOH-treated $\text{TiO}_2$	–	10	300 W Xenon lamp	20	150	–	Hou <i>et al.</i> (2018)
Fenton-mediated-3% AK- $\text{TiO}_2$ -Nps	5	10	18 W UV-LED	50	90	89.15	Present study
$\text{TiO}_2$ (rod)	7	10	100 W Xenon lamp	50	90	25.03	Wahyuni <i>et al.</i> (2018)
$\text{TiO}_2$ -NPs	7	10	30 W UVC lamp	100	150	28	Koysuren & Koysuren (2019)
$\text{TiO}_2$ Nanopowder	11	10	24 W Hitachi black light lamp	30	60	85	Marziyeh <i>et al.</i> (2012)
Commercial $\text{TiO}_2$ particles.	3	$10^{-5}$	UV lamp	70	60	99	Yuangpho <i>et al.</i> (2018)
$\text{H}_2\text{O}_2/\text{TiO}_2$	2	20	39 W/m <sup>2</sup> UV lamp with light intensity	150	80	97.6	Farouq (2018)
$\text{TiO}_2$ -Nps	–	10	Visible	100	150	50	Melinte <i>et al.</i> (2019)
$\text{TiO}_2$ -SF	–	10	300 W Xenon lamp	200	120	54	Xu <i>et al.</i> (2020)
Ti-SA	6	$2 \times 10^{-6}$	400 W UV light	200	180	93.3	Mohammadi & Aliakbarzadeh Karimi (2017)
NF/ $\text{TiO}_2$ -RA		10	150 W high-pressure xenon	10	90	60	Sun <i>et al.</i> (2020)

RA, rhodizonic acid; SS, salicylic acid; Nf, nano fiber; Nr, nano rods; Nps, nanoparticles.

concentration is required for the current study compared to the 10 M NaOH used by Hou *et al.* (2018). However, it is necessary to add that the variation in the light sources from Table 3 greatly influences the efficiency. Hence, at a shorter time and with cost-effective energy, the economically viable nanocatalyst can be applicable for optimal remediation of effluent laden with recalcitrant dyes thereby addressing environmental concerns and contributing to the sustainable development goal (6) clean water and sanitation, goal (7), affordable energy (14) life below water and goal (15) life on land. Furthermore, the modification creates the possibility of recycling and reuse of the photocatalyst without additional treatment due to lowered agglomeration from the alkali enhancement and the conversion of  $\text{Fe}^{3+}$  to  $\text{Fe}^{2+}$  via the capturing of the electron generated from the redox process of the catalyst (AK-TiO<sub>2</sub>-Nps) (Dong *et al.* 2020; Bilici *et al.* 2021). Also, when coupled without other photon-sensitive nanomaterials or immobilized on nanopolymeric support leaching is reduced and a higher recovery yield for reuse is obtainable (Oyetade *et al.* 2022)

## 4. CONCLUSION

In summary, the Fenton-mediated photocatalytic process vis-à-vis the enhanced TiO<sub>2</sub>-Nps was comprehensively evaluated and statistically modeled by the optimization of the independent variable factors for degradation of industrially used azo dye (MB). The XRD result reveals the predominate peak of anatase with rutile, while the SEM imaging indicated modified surface morphology having a mesoporous structure from the BET isotherm. The availability of more pore size and active sites after alkali modification is in tandem with the higher degradation efficiency coupled with the *in situ* mediation of the process by the Fenton reagent to generate more radicals. Furthermore, the study reveals that the slightly acidic pH of the medium enhanced the presence of H<sup>+</sup> ions which increase <sup>-</sup>OH necessary for the generation of the desired hydroxyl radicals. Hence, at a slightly acidic medium, alkali-modified TiO<sub>2</sub>-Nps performs most effectively in the mineralization of organic dye pollutants.

### 4.1. Recommendations

1. The use of Fenton-mediated process at measured effluent concentration influences the efficiency of the process.
2. Development of nanocatalyst trapping system to recover and reuse catalyst for effluent decolorization.
3. Reuse of treated water for basic industrial operations such as desizing, singeing, and cooling of boilers.
4. Development of CO<sub>2</sub> sequestration system to capture the gas resulting in photocatalysis in further industrial process.

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## DATA AVAILABILITY STATEMENT

All relevant data are included in the paper or its Supplementary Information.

## CONFLICT OF INTEREST

The authors declare there is no conflict.

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